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# Removal of Ciprofloxacin Antibiotic from Synthesized Aqueous Solution Using Three Different Metals Nanoparticles Synthesized Through the Green Method

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#### Abstract

This study investigates the possibility of removing ciprofloxacin (CIP) using three types of adsorbent based on greenprepared iron nanoparticles (Fe.NPs), copper nanoparticles (Cu. NPS), and silver nanoparticles (Ag. NPS) from synthesized aqueous solution. They were characterized using different analysis methods. According to the characterization findings, each prepared NPs has the shape of a sphere and with ranges in sizes from of 85, 47, and 32 nanometers and a surface area of 2.1913, 1.6562, and 1.2387 m<sup>2</sup>/g for Fe.NPs, Cu.NPs and Ag.NPs, respectively. The effects of various parameters such as pH, initial CIP concentration, temperature, NPs dosage, and time on CIP removal were investigated through batch experiments. The results showed that 10 mg/L CIP was removed by 100%, 92% and 79% within 180 min using Fe.NPs, Cu.NPs, and Ag.NPs respectively. In addition to this, kinetic models of the adsorption and mechanism of CIP removal were studied. The cinematic analysis demonstrated that adsorption is a physics adsorption mechanism with an energy of 0.846 kJ.mol<sup>-1</sup>, 1.720 kJ.mol<sup>-1</sup>, and 3.872 kJ.mol<sup>-1</sup>, while the low activation energies of 17.660 kJ.mol<sup>-1</sup>, 13.221 kJ.mol<sup>-1</sup>, and 14.060 kJ.mol<sup>-1</sup> for Fe.NPs, Cu.NPs, and Ag.NPs respectively. The kinetic removal process follows a pseudo-first-order model following a physical diffusion-controlled reaction. The data on adsorption was analyzed using the Langmuir, Freundlich, Temkin, and Dubinin models, as well as thermodynamic factors, indicating that the process is appropriate and endothermic sorption. The most practical adsorbent was Fe.NPs

**Keywords:** Removal Ciprofloxacin, Green synthesis, Iron, Copper, Silver, Nanoparticles, Adsorption, Thermodynamics, and Kinetics.

# 1. Introduction

Antibiotic waste in water supplies is one of the most significant challenges facing communities today, especially when it is discovered in drinking water sources [1][2]. The presence of these medicines in large quantities has a negative impact on the ecology [3][4]. In the present time, the world emits harmful substances into the environment either directly or after chemical changes [5]. Antibiotics are widely used because they treat a wide range of bacterial infections in humans, animals, birds, and fish [6].

Ciprofloxacin is a type of antibiotic that is commonly used as a treatment for a variety of bacterial infections around the world [7]. Fluoroquinolones have been found in aquatic environments in concentrations ranging from "1-100 mg/L" [8]. The broad-spectrum fluoroquinolone pharmaceutical medication that is frequently utilized is "Ciprofloxacin ((1 -Cyclopropyl-6-fluoro-4-oxo-7-(piperazine-1-yl)-1,4-dihydroquinoline-3-carboxylic acid hydrochloride hydrate)" [8]. Drug contamination is also caused by trash from hospitals, housekeepers, and human excretion [9]. Non-target persons and biota are at risk from improper disposal of pharmaceutical wastewater antibiotic-loaded [10][11].

Many approaches, such as advanced oxidation processes (AOPs) bioremediation, ozonation, chlorination, and others, have been proposed to treat CIP-contaminated wastewater. However, these methods have a number of drawbacks, including poor removal, difficult procedures, and significant energy needs [1]. Furthermore, multiple studies have suggested that chlorinating antibioticcontaminated wastewater could form а carcinogenic byproduct. As a result, it is crucial to convert antibiotic compounds to safe compounds before discharging them into water systems [12]. treatment approaches Traditional do not completely eradicate antibiotics because of their environmental stability and extended breakdown durations [13] [14]. Antibiotic wastewater treatment necessitates substantial technological resources, with the adsorption process being seen as the most promising method because it is effective, simple to implement, and technically advanced.

To remove pollutant molecules (adsorbates) from contaminated solutions, the procedure employs natural and synthetic materials (sorbents, adsorbents, and biosorbents) [15]. In the adsorption process, the adsorbent material chosen is a critical aspect in obtaining the required efficiency in terms of pollutant removal and cost [16][17]. Before being used, the sorbents must have been tested in this environment to ensure that they can perform adsorption for a variety of pollutants. These tests must also consider the accessibility and costeffectiveness of the tested adsorbents [18][10].

Several materials are available to use as adsorbents, like activated carbon, natural clay (modified bentonite). and polymer-based materials [2]. Researchers have recently proposed using generated trash as an adsorbent in a creative or improved form [20][21]. Metal nanoparticles (NPs) prepared by the green synthesis method using plant extracts have become widely used as adsorbents in the removal of medicine from wastewater [22]. In addition. The green synthesis method is eco-friendly, cost-effective, and easy to develop on a large scale. Green synthesis usually consists of three steps: (1) solvent media selection; (2) environmentally friendly reduction agents' selection; and (3) stable, non-toxic compound nanoparticle selection [19]

Moreover, iron (Fe.NPs) and copper (Cu.NPs) nanoparticles are lower cost, have wide viability [25], simple to produce [26], are environmentally friendly, and have extensive dispersion of reactive surface sites [27] [28], while silver nanoparticles (Ag.NPs) are widely used as antibacterials, sensors, catalysts, and adsorbents [29] [30]. In this study, the adsorption of ciprofloxacin from synthesis wastewater has been successfully employed using Iron nanoparticles (Fe.NPs), Copper nanoparticles (Cu.NPs), and silver nanoparticles (Ag.NPs) nanoparticles have been successfully studied. In addition, "Pseudo-first order. Pseudo-second order, Elovichs, and Behnajady- Modirshahla-Ghanbary (BMG)" models were used to evaluate the adsorption kinetics. The ciprofloxacin analysis was investigated using the Langmuir, Freundlich, Temkin, and Dubinin- models as well as the thermodynamic parameters [31].

# 2. Materials and Methods2.1 Reagents and chemicals

The Ministry of Industry (Ibn Sina Centre) provided the ciprofloxacin used in this study with the characteristics of the drug as (molecular wight = 385.8 g/gmol, color: whit, purity: 99.9% and  $\lambda \max = 276$  nm), while green tea leaves purchased from the local market in Iraq. A spectrophotometer (UV/VIS 1800 SHIMADZU, Japan) was used to

measure the maximum wavelength  $\alpha$  (nm). Figure 1 illustrates the chemical structure of the drug.



Fig. 1. The CIP structure.

# 2.2 Preparation of the Adsorbent

The "Fe.NPs, Cu.NPs, and Ag.NPs" nanoparticles were made using the same processes as those used in earlier investigations [34][35], with the following modifications:

"Green tea" leaf extract was made with "20.0 g of green tea and 300 mL of distilled water (DW). The mixture was preheated on a magnetic stove at 85°C for half an hour. After that the suspended green tea impurities were filtered with" 0.45 µm filter paper and stored at 4°C for further use. By adding 3.25 g of FeC13, 4.996g of CuSO4.5H2O, and 3.4g of AgNO3 salt to 200 mL of DW, a solution of 0.10 M FeCl3, 0.1 M CuSO4.5H2O, and 0.1 M AgNO3 was prepared. After slowly adding the prepared tea extract to each salt solution, the color of each solution changed from light yellow to black for iron, from white to green light for silver, and finally to a dark brown, and from colorless to brownish yellow, and finally to black for copper, the reduction of metal ions to zero valent for example Fe (+3) to Fe (0) when we added the plant extract {this extract is very rich in polyphenols compounds which are played as reducing agents for metal ions}, and from colorless to brownish yellow after that the pH was adjusted to 6 iron [36], 9 for copper and silver [37] [38], and the mixture was continually stirred for 15 minute. The NPs precipitate was collected using vacuum filtration and immediately washed with water and ethanol. Green Fe.NPs, Cu.NPs, and Ag.NPs were dried at room temperature overnight before being ground into fine powders.

#### 2.2 Characterization of NPs

The prepared NPs were characterized using SEM images were taken with a" TESCAN-Vega3

model" to detect morphology and particles size of prepared NPs. The functional groups of Cu, Ag and Fe.NPs were identified by FTIR (IRAffinity, Shimadzu, Japan). A" Brunauer–Emmett–Teller (BET)" application was used to compute the specific surface area, pore size, and pore volume of NPs. Nanoparticle stability was determined using a "zeta potential analysis", and the size and "surface morphology" of the NPs determined by atomic force microscopy (AFM).

#### 2.3 Experiments of Adsorption

Before adding nanoparticles, a stock solution of 10 mg/L of ciprofloxacin solution was prepared, and the pH. A batch of experiments was carried out to examine the adsorption process of ciprofloxacin on prepared NPs. Several operating parameters were met in the studies, including a pH (2-10), a dosage range of 0.1-1 g/L for Fe.NPs, Cu.NPs, and Ag.NPs, a contact time range of up to 180 minutes, contaminant concentrations of (2-15 mg/L), and temperatures of (20-50 °C). The ciprofloxacin solution was supplemented with a particular amount of targeted NPs, and then agitated at 300 rpm in a closed system. 0.1 M H2SO4 and 0.1 M NaOH were used to bring the pH of the CIP solution up to the desired level. The temperature was kept constant, and each parameter's optimal value was recorded. Samples )10 ml( were obtained at various times throughout the experiments, and the change in CIP concentration was determined through a UV/VIS spectrophotometer. The ability of Fe.NPs, Cu.NPs, and Ag.NPs to extract antibiotic pollutants from aqueous solutions was assessed using R% removal efficiency and Qe mg/g adsorbent capacity values using the following two formulas [34] [33].

$$\% Removal = \frac{C_{o} - C_{t}}{C_{o}} \times 100 \qquad \dots (1)$$

$$Q_e = (C_o - C_e) \times \left(\frac{V}{W}\right) \qquad \dots (2)$$

Where  $C_o$  is initial CIP concentration (mg/L),  $C_t$  is the concentration after adsorption being start (mg/L) and  $C_e$  is equilibrium concentration (mg/L). V is the volume of CIP solution (L) and W is the Wight of CIP (g).

# Results and Discussions Characterization of NPs

A scanning electron microscope (SEM) was used to illustrate the shape and distribution of the

nanoparticles. According to the SEM of Fe.NPs that is presented in Figure (2a), the adsorbent surface is rough and contains many different disorganized aggregates. On the surface of the Fe.NPs wall, there were a number of grooves and deep ravines. The morphologic characteristics of the surface of the Fe.NPs are generally favorable because they offer active sites and a large surface area for the molecules that are adsorbed. Figures

(2b-c) show SEM images of the generated Cu.NP and silver nanoparticles (Ag-NP). SEM pictures revealed the shape and distribution of these components. Because polyphenols are present on the surface of nanoparticles, irrelevant spherical nanoparticles were discovered that were compatible with copperand silver-based preparations employing extracts of green tea leaves



Fig. 2. Scanning electron microscope (SEM) micrograph of (a) Fe.NPs, (b) Cu.NPs, and (c) Ag.NPs

The Fe.NPs FTIR spectrum is shown in Figure 3a. The "FTIR analysis of Fe.NPs reveals a functional group of O - H at 3364 cm-1, indicating the existence of polyphenols [25] and the C=O appeared at 1635 cm-1 also referring to the presence of polyphenols. The functional groups of C-H, C-O-C and C=C appeared at 2924 cm-1, 1035 cm-1, and 1367 cm-1 belong to the oxidized polyphenols on the produced Fe.NPs. Polyphenols are thought to behave as antioxidants in Green Tea Extract as well. In the FTIR analysis of Cu.NPs Figure (3b), the presence of polyphenols is indicated by this the peak at 3411 cm-1 that belong to O-H stretching, along with the association

between C-H asymmetrical stretching and certain signals in 2948, 1782, 1615, and 1029 cm-1, C=O of aromatic rings, C=C stretch, and C-OH bending respectively. Based on FTIR measurements, Ag.NPs with a wave range of 3371cm-1 to 1021cm-1 show characteristic peaks. Wide and strong absorption peaks were identified between 3371 and 3259 cm-1, indicating the presence of polyphenols and extended hydroxyl vibrations (O-H). Carbonyl C=O was detected by a significant absorption, with C=C stretching frequencies peaking between 1639 and 1634 cm-1. Figure 3c shows the vibration of the O-H delay, which could be caused by the other pits between 1160cm-1.



Fig. 3. FTIR spectrum of (a) Fe.NPs, (b) Cu.NPs, and (c) Ag.NPs nanoparticles.

The size and surface morphology of Fe.NPs, Cu.NPs, and Ag.NPs nanoparticles were investigated with the help of a atomic force microscopy (AFM). The average nanoparticle size

for according to the AFM for iron, copper, and silver nanoparticles were (85, 47, and 32 nm), respectively, as shown in Figures (4a-c). Figures









Fig. 4. AFM images of nanoparticles composed of (a) Fe.NPs, (b) Cu.NPs, and (c) Ag.NPs.



Fig. 5. Nanoparticles of (a) Fe.NPs, (b) Cu.NPs, and (c) Ag.NPs examined by atomic force microscopy.

Nanofluid stability was determined using a zeta potential analysis technique, as shown in Figure 6ac, the zeta potential values were -19.34 mV for Fe.NPs, -17.5 mV for Cu.NPs, and -29.1 mV for Ag.NPs, it was proven that the nanoparticles were more agglomerative.



Fig. 6. Zeta potential of (a) Fe.NPs, (b) Cu.NPs, and (c) Ag.NPs nanoparticles.

Blumenauer-Emmer-Teller (BET) data are shown in Table 1, which explain and clarify the surface area. Pore sizes for iron, copper, and silver nanoparticles were 34.8651 nm, 8.2568 nm, and 5.1843 nm, respectively. According to the IUPAC, pore sizes between 20 and 50 nm are considered mesoporous.

Nanoparticle	BET parameters BET(m <sup>2</sup> /gm)	Volume of pores(cm <sup>3</sup> /gm)	Size of pores (nm)
Fe.NPs	2.1913	0.0191	34.8651
Cu.NPs	1.6562	0.00839	8.2568
Ag.NPs	1.2387	0.000618	5.1843

 Table 1,

 The BET parameters for Fe.NPs, Cu.NPs, and Ag.NPs nanoparticles.

#### 3.2 CIP removal under various conditions

In a closed system, the removal of ciprofloxacin by Fe.NPs, Cu.NPs, and Ag.NPs" was studied, and the removal percentage was determined under various experimental conditions. UV-Vis at a wavelength of 276 nm was used to take samples and analyze them at various time intervals. "Initial pH was set to 2.5, 3, 4, 5, 7, 8, 9, and 10, initial ciprofloxacin concentrations were set to 2, 5, 10, and 15 mg/L, Fe.NPs, Cu.NPs, and Ag.NPs doses were set to 0.1, 0.25, 0.5, 0.75, and 1 g/L, and the solution temperatures were set to 20, 30, 40, and 50 °C. Eq. 1 was used to determine the ciprofloxacin removal performance.

#### 3.2.1 Effect of adsorbent

The adsorbent dosage is an important factor to consider due to its role in demonstrating the

catalyst's capacity to deal with a particular initial contaminant concentration. The effect of Fe.NPs, Cu.NPs, and Ag.NPs dosages on ciprofloxacin elimination is shown in Figures 7a-c, respectively. The ciprofloxacin removal was raised from 18% to 70% when Fe.NPs were used, and the adsorption dosage was increased from 0.1 to 1.0 g/L, while it improved from 20% to 54% when Cu.NPs were used, and from 18% to 45% when Ag.NPs were used. Higher Fe.NPs, Cu.NPs, and Ag.NPs for ciprofloxacin adsorption improved the removal rate and effectiveness while maintaining the other parameters (drug concentration, pH, temperature, and contact time). This is because the total area and active site have both increased. [41]. For iron. copper, and silver nanoparticles, doses of 0.5g/L, 0.75g/L, and 1 g/L were chosen as the optimal values. A similar result was indicated by [3], [4].



Fig. 7. Effect of "(a) Fe.NPs , (b) Cu -NPs, and (c) Ag.NPs doses at pH =3, 10 mg / L ciprofloxacin, 40°C, 300 rpm and contact time of 60 min".

#### **3.2.2 Effect of temperature**

At temperatures ranging from 20 to 50 °C, the influences on ciprofloxacin removal efficiency were investigated. The efficiency of ciprofloxacin at various temperatures is shown in Figures 8 a-c. Since Fe.NPs removed 36 percent, 40 percent, 54 percent, and 53 percent of ciprofloxacin at 20, 30, 40, and 50°C, respectively, 43 percent, 44 percent, 78 percent, and 49 percent with Cu.NPs, and Ag.NPs removed 31 percent, 40 percent, 52 percent, and 45 percent with Ag.NPs, it is possible to conclude that the removal rate of ciprofloxacin

is influenced by temperature and increased with increase in temperature. This could be due to an increase in the number of sorption sites generated because of the breaking of some internal bonds near the active surface sites of the adsorbent. Furthermore, the increasing temperature may increase the mobility of the CIP, enabling it to penetrate further. As a result, there are more medicines interacting with adsorbent active surfaces." For Fe.NPs, Cu.NPs, and Ag.NPs", the temperature was 40°C. Similar optimal observations were noted by [5].



Fig. 8. The temperature effect on ciprofloxacin removal onto various adsorbents at (10 mg/L of CIP), 300 rpm, one hours (a) 0.5 g/L and pH=10 of Fe.NPs, (b) 0.75 g/L and pH=4 of Cu.NPs, and (c) 1 g/L, and pH=4 of Ag.NPs.

#### 3.2.3 Effect of pH

As shown in Figures (9 a-c), the influence of pH is compared to ciprofloxacin adsorption by NPs. Two reasons were identified in the studies as possibly accounting for the increased ciprofloxacin adsorption: (1) At low pH, the concentrations of H+ in the solution were very high, enhancing the electrostatic pull between H+ in the solution and the adsorption sites between H+ and CIP+; (2) at higher (pH10), H+ of active groups can be easily dissociated and provide more adsorption sites [44].

In acidic environments, antibiotic molecules are positive, with 99% of ciprofloxacin molecules being (cationic), 10% being ciprofloxacin +, and 95% being anionic. When the pH is 7, ciprofloxacin 0" predominates (zwitterion). A physi-sorption reaction between ciprofloxacin molecules and the active sites of" Fe.NPs, Cu.NPs, and Ag.NPs "may occur at pH = 10, 4, and 4, respectively. Figure (9 a) demonstrates that Fe.NPs improved the efficacy of removal at a range of pH values (2.5, 3, 4, 5, 7, 8, 9, and 10) for 60 min, with increases of 21%, 54%, 69%, 72%, 70%, 68%, 81%, and 92%, respectively. While Figure (9 b) showed that the percentage removal of ciprofloxacin by Cu.NPs increased at acidic pH and then decreased at basic pH as 36 percent, 51 percent, 78 percent, 50 percent, 43 percent, and 32 percent, a similar result was indicated by [6], [7], [8]. Figure (9 c) explains the removal of

ciprofloxacin by Ag.NPs and the same observation was made at 37%, 45%, 52%, 48%, 43%, 30%, 23%, and 21%. The optimum values of pH for the removal" ciprofloxacin by Fe.NPs, Cu.NPs, and Ag.NPs are 10, 4, and 4" respectively.



Fig. 9. The effect of pH on the removal of " ciprofloxacin at 10 mg/L of concentration", one hours, and 300 RPM onto (a) 0.5 g/L, pH10 and 40°C of Fe.NPs, (b) 0.75 g/L, pH 4, and 40°C of Cu.NPs, (c) 1 g/L, pH4, and 40°C.

#### 3.2.4 Effect of initial concentration

Figures (10 a-c) represent the effect of drug concentration on removal efficiency for ciprofloxacin adsorption in the range of 2, 5, 10, and 15 mg/L. By employing "Fe.NPs, Cu.NPs, and Ag.NPs", the removal percentage decreased from 100% to 81% ,81% to 39 % for Fe.NPs, while Cu.NPs showed 99 % to 83 %, 78 % to 42 %, and Ag.NPs removal efficiency decreased from 57 % to 54 %, 52 %, to 48 % as the concentration of ciprofloxacin increased. Other researchers'

observations [34] have similar results to this study. The initial ciprofloxacin concentration for more active sites of Fe.NPs, Cu.NPs, and Ag.NPs because they are likely to rise, resulting in ciprofloxacin molecule adsorption competition [42]. The driving force is accelerated, and the resistance to mass transfer is reduced, when the first concentration is high. Within one hour of the process, the optimal value for the initial CIP concentration with all adsorbents was "10mg/L", and the removal of ciprofloxacin was 81 %, 78 %, and 54 %.



Fig. 10. The effect of the ciprofloxacin concentration at 300 rpm, one hour, and  $T = 40^{\circ}C$  (a) Fe- NPs of 0.5g/L, pH10, (b) Cu.NPs of 0.75g/L, pH4, and (c) Ag.NPs of 1g/L, pH4.

## 3.2.5 Effect of contact time

To indicate the equilibrium point, a time effect is an important parameter of the sorption process. At pH 4, 7, and 10, the effect of increased contact time is seen in Figure 11. With more time, the batch system's ciprofloxacin removal efficiency improves. The process was initially fast because of the high driving force at high ciprofloxacin level, but when the amount of non-adsorbed " ciprofloxacin "molecules in the adsorbent active site decreased, the removal rate declined for all pH levels [49]. The " ciprofloxacin removal" at pH 4, 7, and 10 for one hour was "59%, 72%, and 81% by using Fe.NPs, and 80%, 43%, and 27% for Cu.NPs", while the removal of ciprofloxacin was 53%, 43%, and 22% for Ag.NPs. The " ciprofloxacin removal after 180 min. at 4, 7, and 10" were 92%, 93%, and 100% with Fe.NPs, and 92%, 70%, and 50% with Cu.NPs, while the removal efficiency was 79%, 67%, and 42% by using Ag.NPs.



Fig. 11. Time effect at different pH (CIP conc.10 mg/L, 0.5 g/L Fe.NPs, 0.75 g/L Cu.NPs, and 1 g/L Ag.NPs, with constant temperature of 40 °C.

#### 4. Adsorption Mechanism

Equations (3) and (4) were used to determine the mechanism of the sorption process. (3) and (4) [9][5] [10].

### Kinetics of intraparticle diffusion:

$$q_{t = K_{id} t^{0.5} + C}$$
 ...(3)  
Kinetic model of liquid film diffusion:

$$Ln \frac{1-q_t}{q_e} = -K_{fd} \times t \qquad \dots (4)$$

The intraparticle diffusion constants are Kid (mg/g min0.5) and C (mg/g). The thickness of the boundary layer is indicated by the C parameter, while the liquid film diffusion constant is shown by  $K_{fd}$  (m<sup>-1</sup>). When the linear trend fit from the qt vs t<sup>0.5</sup> as presented in Figures (12a-c) passes the point of origin of the parameter C = 0, that mean the intraparticle diffusion is the limiting rate. In Figure

(12a-c), the slop and intercept of the plot of ln (1qt/qe) versus t correspond to K<sub>fd</sub> and C. Tables (2), (3), and (4) demonstrate the results of "intraparticle and film diffusion" experiments at different ciprofloxacin initial concentrations (4). The linear model in Figures (12a-c) and (13a-c) did not pass through the origin, implying that the thickness of the boundary layer controls the adsorption process. The high values of the regression coefficients suggest that liquid film diffusion plays a more crucial role, and that a greater concentration gradient causes ciprofloxacin molecules to diffuse more quickly across the boundary layer surrounding the adsorbent. The C values strongly suggest that intr-aparticle diffusion was also utilized in the sorption process. In addition to diffusion. several adsorption mechanisms control the rate of intra-particle diffusion. Such aberrations have been described in a number of scientific studies [51], [10].

CIP	Intra-par	ion	Liquid Film Diffusion			
(mg/L)	Kid	C(mg/g)	R <sup>2</sup>	Kfd	C(mg/g)	R <sup>2</sup>
	(mg/g.min <sup>0.5</sup> )			(min <sup>-1</sup> )		
15	1.2389	-0.3418	0.995	0.0074	-0.0581	0.9644
10	1.7863	-0.6041	0.9937	0.0186	-0.066	0.9933
5	0.9729	0.7791	0.9675	0.022	-0.2507	0.9414
2	0.4327	0.6789	0.8761	0.0467	-0.4272	0.8984
Average			0.9580			0.9503
R <sup>2</sup>						

#### Table 2,

Model and liquid film diffusion on Fe.NPs at different CIP conc. for the intra-particle adsorption mechanism.

#### Table 3,

Model and liquid film diffusion on Cu.NPs at different CIP concentrations for the intra-particle adsorption mechanism.

CIP (mg L <sup>-1</sup> )	Intra-particle Diffusion			Liquid Film Diffusion			
	$\frac{\mathbf{K}_{\mathrm{id}}(\mathrm{mg}\;\mathrm{g}^{-1}.\mathrm{min}^{-1})}{^{0.5})}$	C(mg/g)	$\mathbb{R}^2$	$\mathbf{K}_{\mathrm{fd}} (\min^{-1})$	C(mg. g <sup>-1</sup> )	$\mathbf{R}^2$	
15	0.7982	0.0498	0.9727	0.0318	-0.1481	0.9584	
10	1.349	0.3249	0.9963	0.0308	-0.0212	0.9834	
5	1.4592	0.1978	0.9931	0.0341	-0.1047	0.9926	
2	1.6584	0.559	0.9895	0.0398	-0.0662	0.9475	
Average R <sup>2</sup>			0.9879			0.9704	

#### Table 4,

Model and liquid film diffusion on Ag.NPs at different CIP conc. for the intra-particle adsorption mechanism.

СІР	Intra-j	particle Di	ffusion	Liquid Film Diffusion			
(mg/L)	K <sub>id</sub> (mg /	C(mg	R <sup>2</sup>	K <sub>fd</sub> (min <sup>-1</sup> )	C(mg	R <sup>2</sup>	
	g.min <sup>0.5</sup> )	/g)			/g)		
15	0.8465	-0.358	0.979	0.0257	-0.0521	0.9848	
10	0.7216	-0.0958	0.9826	0.0298	-0.0952	0.9813	
5	0.719	0.3928	0.9731	0.0681	-0.1973	0.9852	
2	0.6123	0.4693	0.9594	0.0405	-0.2339	0.9801	
Average			0.9735			0.9828	
R <sup>2</sup>							



Fig. 12. The intraparticle diffusion at a different initial concentration of CIP adsorption (Temp 40C, 300 rpm, and 60 min) onto (a) Fe.NPs adsorbent dose of 0.5 g, pH10.(b) Cu.NPs sorbent dose of 0.75 g, pH4, and (c)Ag.NPs sorbent dose of 1 g, pH4.



Fig. 13. The liquid diffusion at a various concentration of CIP adsorption (Temp 40C, 300 rpm, and 60 min) onto (a) Fe.NPs adsorbent dose of 0.5 g, pH10.(b) Cu.NPs adsorbent dose of 0.75 g, pH4, and (c)Ag.NPs adsorbent dose of 1 g, pH4.

#### 5. Adsorption Isotherm

Langmuir, Freundlich, Temkin, [52][47] and Dubinin Isotherm [53] [22], have all modeled ciprofloxacin; the equations for these models are listed below.

Langmuir:  

$$\frac{1}{q_e} = \frac{1}{q_{max}} K_L \left(\frac{1}{C_e}\right) + \frac{1}{q_{max}} \dots (5)$$
Separation factor or dimensionless constant (RL)

1

$$R_L = \frac{1}{1 + bC_o} \qquad \dots (6)$$
  
Freundlich:

$$Log q_e = \frac{1}{n} \log C_e + \log K_F \qquad \dots (7)$$

Temkin:

$$q_e = \frac{R_T}{B_T} \ln C_e + \frac{R_T}{B_T} \ln K_F \qquad \dots (8)$$

$$\ln q_e = \ln q_m - \beta \varepsilon^2$$

$$\xi = \ln RT \left(1 + \frac{1}{c_e}\right)$$
 ...(10)

$$E + \frac{1}{\sqrt{-2\beta}} \qquad \dots (11)$$

#### **5.1 Langmuir model**

Figure (14a-c) shows the plots of various models, where qmax and kL are constants of

Langmuir model. These values were calculated using the slope and intercept of the presented graph, 1/qe vs 1/Ce. As demonstrated in Tables (5), (6), and (7), Langmuir isotherms define the values where (R2) Langmuir is greater than other models and homogenous adsorbent surfaces with the very same adsorbent surface are in Langmuir (7). Tables (5), (6), and (7) illustrate the constant b of Langmuir, which was set at 25.125 for Fe.NPs, 22.0925 for Cu.NPs, and 0.3643 for Ag.NPs (7). When (RL > 1), linear (RL = 1), favorable (RL 1), or irreversible (RL = 0), RL is a dimensionless constant and is commonly used as a separating factor for the RL indicator values and unfavorable adsorption. The RL values for CIP adsorption on "Fe.NPs, Cu.NPs, and Ag.NPs were (0.02217-0.0033), (0.00452-0.00451), and (0.2504-0.1793), respectively, and while these values indicated favorable CIP adsorption on adsorbents, they also gave erroneous values between 0 and 1. The maximal absorption (qmax.) of CIP per gram of Fe.NPs, Cu.NPs, and Ag.NPs was 9.95024, 8.3822, and 8.5034mg, respectively. For all adsorbents, the data fit well with the Langmuir isotherm, indicating a homogeneous surface supply of active sites on the adsorbent. A similar observation was reported by [11] [3].



... (9)

Fig. 14. The plot showing the Langmuir isotherm model at a different initial concentration of CIP adsorption (Temp 40C, 300 rpm, and 60 min) onto (a) Fe.NPs dose of 0.5 g, pH10.(b) Cu.NPs dose of 0.75 g, pH4, and (c)Ag.NPs dose of 1 g, pH4.

#### 5.2 Freundlich isotherm model

The Freundlich isotherm is an experimental equation that considers a multi-layer sorption system on a heterogeneous surface, with the values )kF( and n confirming favorable sorption. From the plotted graph of log qe vs. log Ce, the slope and intercept were estimated as shown in Figure (15a-

c). The n constants affect adsorption favorability, and " values of n between 2 and 10 are generally satisfactory, while values between 1 and 2 are difficult, and adsorption characteristics less than 1 indicate poor adsorption" (n = 4.9417, 4.7236, 2.7078) as shown in Tables (9), (10), (11) indicate acceptable adsorption [51].



Fig. 15. The plot showing the Freundlich isotherm model at a different initial concentration of CIP adsorption (Temp 40C, 300 rpm, and 60 min) onto (a) Fe.NPs dose of 0.5 g, pH10.(b) Cu.NPs dose of 0.75 g, pH4, and (c)Ag.NPs dose of 1 g, pH4.

#### 5.3 Temkin isotherm model

The maximum binding energy and heat of sorption coefficients are "KT (L/g) and BT (kJ/mol)". The slope and intercept of a plotted qe graph vs. In Ce were used to get the KT and BT values (16a-c). The KT and BT values represent

minute changes in sorption heat and solid interactions between adsorbent and adsorbate, as seen in Tables (8), (9), and (10).. Tables (8), (9), and (10), together with the required coefficient of correlation, and the low correlation coefficient R2 indicates that the model has no applicability.





Fig. 16. The plot showing the Temkin isotherm model at a different initial concentration of CIP adsorption (Temp 40C, 300 rpm, and 60 min) onto (a) Fe.NPs sorbent dose of 0.5 g, pH10.(b) Cu.NPs sorbent dose of 0.75 g, pH4, and (c)Ag.NPs adsorbent dose of 1 g, pH4.

#### 5.4 Dubinin isotherm model

As demonstrated in Tables (5), (6), and (7), The values qe and describe the degree and mean sorption energy per mole of adsorbate, which may be calculated from the slope and intercept of the graph plotted at ln qe versus  $\xi 2$ . Figure (17a-c). For "Fe.NPs, Cu.NPs, and Ag.NPs", the E values were (0.8461, 1.7205, and 3.8727 kJ/ mol, respectively, indicating physical adsorption E8 kJ/ mol, while E

lies between (8-16) denotes chemical adsorption [55][56]. Because the R2 value is higher for all adsorbents, we can use this model. Figures (15a-c), (16a-c), (17a-c), and (18a-c) show the "adsorption isotherms" derived by four models, as well as "CIP experimental" data, and it is obvious that the Langmuir and Dubinin techniques were closer fits in terms of R2.



Fig. 17. The plot showing the Dubinin isotherm model at a different concentration of CIP adsorption (Temp 40C, 300 rpm, and 60 min) onto (a) Fe.NPs dose of 0.5 g, pH10.(b) Cu.NPs dose of 0.75 g, pH4, and (c)Ag.NPs dose of 1 g, pH4

Isotherm parameters va Langmuir	alues of Fe-NPs.		Froundlich		
$q_{max}$ (mg g <sup>-1</sup> )	<b>B</b> (L mg <sup>-1</sup> )	$\mathbf{R}^2$	k <sub>F</sub>	n	$\mathbf{R}^2$
9.95	25.13	0.947	8.287	4.941	0.755
Temkin			Dubinin		
$K_T(L/g)$	B <sub>T</sub> (kJ/mol)	$\mathbf{R}^2$	Qm (µg/g)	E (kJ/mol)	$\mathbb{R}^2$
7.029	0.258	0.5837	1.141	0.846	0.986

# Table 5,

Table 6,

0.167

Isotherm parameters values of Cu-NPs.

Langmuir			Freundlich		
$q_{max}$ (mg g <sup>-1</sup> )	<b>B</b> (L mg <sup>-1</sup> )	$\mathbf{R}^2$	$\mathbf{k}_{\mathbf{F}}$	n	$\mathbb{R}^2$
8.3822	22.0925	0.9245	0.1512	4.7236	0.6602
Temkin			Dubinin		
$K_T(L/g)$	B <sub>T</sub> (kJ/mol)	$\mathbb{R}^2$	Qm (µg/g)	E (kJ/mol)	$\mathbb{R}^2$
40.4976	6.8995	0.8064	1.1009	1.7205	0.8955
Langmuir	rs values of Ag-NPs.		Freundlich		
Langmuir			Freundlich		
$q_{max}$ (mg g <sup>-1</sup> )	<b>B</b> ( <b>L</b> mg <sup>-1</sup> )	$\mathbf{R}^2$	$\mathbf{k}_{\mathbf{F}}$	n	$\mathbf{R}^2$
8.503	0.363	0.903	3.013	2.708	0.907
Temkin			Dubinin		
$K_T(L/g)$	B <sub>T</sub> (kJ/mol)	$\mathbf{R}^2$	Qm (µg/g)	E (kJ/mol)	$\mathbf{R}^2$

1.033

0.908

# 6. Adsorption Thermodynamic

At 298, 303, 313, and 323 K, the adsorption behaviors of various concentrations of" CIP onto Fe.NPs, Cu.NPs, and Ag.NPs" were censoriously investigated, and the thermodynamic parameters of Gibbs free energy ,entropy and enthalpy were obtained using equations 12 to 16. [56], [57]:

3.155

$\Delta G \circ = -RT \ln K_c$	(12)
$q_e$	

$$K_c = \frac{\pi e}{C_e} \qquad \dots (13)$$

$$\Delta G \circ = \Delta H - T. \Delta S \circ \dots (14)$$

$$\ln \frac{c_t}{C \circ} = -k_{obs}t \qquad \dots (15)$$

$$\ln K_{obs} = \ln A - \frac{E_a}{RT} \qquad \dots (16)$$

Using ln Kc values for various temperatures, the Gibbs free energy ( $\Delta$ G0) was calculated. According to Eq.19, the slope and intercept at  $\Delta$ H0 and  $\Delta$ S0 of the graph of  $\Delta$ G0 vs T. Figure can be used to determine "enthalpy ( $\Delta$ H0) and entropy ( $\Delta$ S0)" (18a-c). Tables (8), (9), and (10) show the free energy, enthalpy, and entropy values for iron,

copper, and silver nanoparticles. The positive enthalpy ( $\Delta$ H0) value demonstrated endothermic sorption and favorable, indicating the spontaneous nature of CIP adsorption onto Fe.NPs, Cu.NPs, and Ag.NPs [58], [56]. During the adsorption process, positive entropy change determines the increase in disruption at liquid / solid interfaces [58]. Eq.16 was used to compute the activation energy, in which A represents the "Arrhenius factor, R represents the gas constant (8.314 J / mol.K)", K represents the temperature in kelvin, Ea represents the activation energy (kJ/mol), and kobs (min-1) represents the rate constant Eq.15 [59], [34]. The intercept and slope of ln (Ct/C0) and the time t (min) were used to calculate these values. For "Fe.NPs, Cu.NPs, and Ag.NPs", the straight line of In kobs versus 1 / T Figure (19a-c) deviates by" 17.66 kJ / mol, 13.22 kJ / mol, and 14.06 kJ / mol", respectively, Diffusion-controlled processes are indicated by an activation energy (Ea) value greater than 21 kJ / mol, whereas chemically controlled processes are indicated by an Ea value less than 21 kJ / mol. [59].

3.873

0.991



Fig.18. Relationship between  $\Delta G^0$  and T of CIP adsorption onto (a) "Fe.NPs at initial concentrations of 10 mg/L, pH=10, and 300 rpm for adsorption of CIP with a dose of 0.5 g and 60 min, (b) Cu.NPs at initial concentrations of 10 mg / L, pH=4, and 300 rpm for adsorption of CIP with a dose of 0.75 g"



Fig. 19. "Relationship between ln kob against 1 / T to caculate Ea at concentrations of 10 mg / L, and 300 RPM, 60 min for adsorption dose of CIP on to (a) Fe.NPs with a dose of 0.5 g and pH10, (b) Cu.NPs with a dose of 0.75 g and pH4, and (c) Ag.NPs with a dose of 1 g and pH4"

#### Table 8,

Thermodynamic study of CIP adsorption onto Fe.NPs (CIP Conc.=10 mg/L	, Fe.NPs dosage = 0.5 g, contact time=
60 min, and pH=10).	

$\Delta G^0$ (KJ/mol	l)		$\Delta H^0 (KJ/mol)$	$\Delta S^0 (KJ/mol.K)$	
T=20°C	T=30°C	T=40°C	T=50°C	21.067	0.073
-0.367	-0.749	-2.249	-2.301		

Table 9,

Thermodynamic study of CIP adsorption onto Cu.NPs (CIP conc.= 10 mg/L, Cu.NPs dosage= 0.75 g, contact time= 60 min, and pH=4).

$\Delta \mathbf{G}^{0} \left( \mathbf{KJ/mol} \right)$				$\Delta \mathbf{H}^{0} \left( \mathbf{KJ/mol} \right)$	$\Delta S^0 (KJ/mol.K)$
T=20°C	T=30°C	T=40°C	T=50°C	17.544	0.061
-0.017	-0.069	-4.108	-0.701		

Table 10,

Thermodynamic study of CIP adsorption onto Ag.NPs (CIP conc.=10 mg/L, Ag.NPs dosage= 1 g, contact time= 60 min, and pH=4).

$\Delta \mathbf{G}^{0} \left( \mathbf{KJ/mol} \right)$				$\Delta \mathbf{H}^{0} \left( \mathbf{KJ/mol} \right)$	$\Delta S^0 (KJ/mol.K)$
T=20°C	T=30°C	T=40°C	T=50°C	12.713	0.042
0.516	-0.069	-0.959	-0.593		

# 5. Conclusions

Three adsorbents Fe.NPs, Cu.NPs, and Ag.NPs were characterized using advanced techniques such as SEM, AFM, BET, zeta potentials, and FT-IR, with the results indicating that nanoparticles had favorable effects in the adsorption process. Several parameters were studied to optimize the adsorption process, including, contact time, pH, temperature, and initial antibiotic concentration, and the best value of this parameter was pH10, 60 min, 10 mg/L, 40°C, and 0.5 g/L dosages for Fe.NPs, pH4, 60 min, 10 mg/L, 40°C, and 0.75 g/L for Cu.NPs, and finally pH4, 60 min, 10 mg/L, 40°C, and 0.75 g/L for Ag.NPs. The isothermal study showed the best-fitting models for the adsorbent Fe.NPs and Cu.NPs were the Langmuir and Dubinin models, respectively, whereas the best-fitting models for the adsorbent Ag.NPs were the Dubinin and Temkin models. Both the endothermal nature and the spontaneous nature of the sorption process were mentioned by the thermodynamic element. When  $\Delta G0$  is negative, the nature of adsorption was spontaneous and feasible for all nanoparticles. Finally, Fe.NPs was the most appropriate adsorbent compared with Cu.NPs and Ag.NPs in the order of "Fe.NPs > Cu.NPs > Ag.NPs".

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# إزالة المضاد الحيوي السيبروفلوكساسين من المحلول المائي باستخدام ثلاث جسيمات نانوية معدنية تم تصنيعها بالطريقة الخضراء

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# الخلاصة

تبحث هذه الدراسة إمكانية إز الة السيبر وفلو كساسين (CIP) من محلول مائي باستخدام ثلاثة أنواع من الجسيمات النانوية (Ag. NPS). تم توصيف الجسيمات النانوية مثل جسيمات الحديد النانوية (Fe. NPs) وجسيمات النحاس النانوية (Cu. NPS) وجسيمات الفضة النانوية (Ag. NPS). تم توصيف الجسيمات النانوية المحضر ة باستخدام طرق تحليل مختلفة ووفقًا لنتائج التوصيف فأن الجسيمات النانوية التي تم تحضير ها تمتلك شكل كرة وبأحجام تتر اوح من 85 و 47 و 22 نانومترًا ومساحة سطحها 2.1913 و 1.6562 و 1.2387 متر مربع / غرام لكل من NPs ، Fe. NPs و Cu. NPs ، على التوالي. تمت دراسة تأثيرات العوامل المختلفة على إز الة السيبر وفلو كساسين مثل الأس الهيدر وجيني والتركيز الأولي للسيبر وفلو كساسين ودرجة الحرارة وجرعة الجسيمات النانوية والوقت. أظهرت النتائج أنه تمت إز الة السيبر وفلو كساسين مثل الأس الهيدر وجيني والتركيز الأولي للسيبر وفلو كساسين ودرجة الحرارة وجرعة الجسيمات النانوية والوقت. أظهرت النتائج أنه تمت إز الة 10 ملغرام / لتر من السيبر وفلو كساسين بنسبة 100 / و 29 رو 70. خلال 100 دقيقة باستخدام 100 ملغران و المعرام المختلة و مالوقت. أظهرت النتائج أنه تمت إز الذه 10 ملغرام / لتر من السيبر وفلو كساسين بنسبة 100 / و 29. و 70. خلال 100 دقيقة باستخدام 200 عن 200 مالي و الوقت. أطهرت النتائج أنه منه 100 ملغرام / لتر من السيبر وفلو كساسين وألي و 100 ملغرام النانوية و 200 ملغري النتائج الذه الميبر وفلو كسامين معال الأس الهيدر وجيني والتركيز الأولي السيبر وفلو كساسين و درجة الحرارة وجرعة الجسيمات النانوية و الوقت. أطهرت النتائج أنه تمت إز الذ 10 ملغرام / لتر من السيبر وفلو كساسين بنسبة 100 / و 29. و 79. خلال 100 دقيقة باستخدام 200 ملو 200 كانت فيزيانية بطاقة مالغران و 10.00 ملو و 10.00 كانت فيزيانية بطاقة 2.000 كلو معرا مول و 20.00 معلو مول مول و 200 معليه ولو / مول و 200 مولي بولي إز الة السيبر وفلو كساسين وأظهر الدراسات أن الية الامتز از كلت فيزيانية بطاقة 2.000 كلو مول مان من 200 مال مول و 200 مول مول مول / مول بينما طقات التنشيط 2.000 كليل وول / مول و 200 مول و 200 مول و 200 مالغران و 200 مول و 200 مول مول مول من مال مال معرا و 200 مالغوالي. تشير دراسة ولي يز در المة الي ور يخضع لنموزجا من الدرجة الأولي. الو ول لمول مان مما مالة مول مول مول مول مول مول مول